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Investigation of Performance of Organic Rankine Cycle-Vapor Compression Refrigeration System Using Different Refrigerant

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***Abstract*- In this study, the energy and exergy analysis of a combined cycle was carried out. This cycle consists of an organic Rankine cycle and a vapor compression refrigeration cycle for producing the cooling effect. Four organic fluids were used as working fluids such as R600a, R245fa, RC318 and R236fa. The parametric analysis allowed us to characterize the combined system and to study the effect of some parameters that were used to estimate the thermal and exergy efficiency of the studied system. The results showed that the operating parameters have a significant impact on the performance of the combined system. Due to environmental issues of R600a is recommended as a superior candidate for the ORC-VCR system for retrieving low-grade thermal energy.On the other hand, the results of the exergydestruction distribution showed also that maximum exergy destruction rate is found in R600a and minimum is in RC318.**

***Keywords*- Rankine cycle, refrigeration, exergy, organic fluids.**

I. INTRODUCTION

Nowadays, there are numerous attempts in the utilization of renewable energies such as geothermal heat, wind energy, and solar energy as clean energy sources for electricity production or cooling processes. Also, waste heat can be considered as renewable and clean energy, since it is free energy and there is no direct carbon emission. Waste heat can be rejected at a wide range of temperatures depending on the industrial processes [1].

An ejector refrigeration system and an absorption refrigeration system can be activated by thermal energy source with a temperature range from 100 to 200 °C. They have several advantages such as simple structure, reliability, low investment cost, slight maintenance, long lifetime, and low running cost [2, 3].

Nevertheless, they are not appropriate for thermal sources less than 90 °C and are also not appropriate for working in high-temperature surroundings. Furthermore, the minimum cooling temperature could be achieved by both systems is 5 °C [4].

The working fluid selection has a large influence on the performance of combined organic Rankine cycle-vapor compression refrigeration (ORC-VCR) system. Several studies have been done on the working fluid selection, i.e. R12, R22, R113, and R114 for the ORC-VCR system and identified the most suitable one, which may yield highest coefficient of performance (COP) [8–13]. The refrigerants R123, R134a, and R245ca were evaluated to find the best one for the ORCVCR system by Aphornratana and Sriveerakul [14]. The results indicated that R123 achieves the best system performance.An ORC-VCR system activated by a low temperature source utilizes R134a was analysed by Kim and Perez-Blanco [4].

The minimum cooling temperature could be achieved by the system was -10 °C. An ORC-VCR system utilizing two different candidates for the power and refrigeration cycles, i.e. R245fa and R134a, respectively was investigated by Wang et al. [1].

The system coefficient of performance (COPS) attained approximately 0.5. Six candidates, namely R134a, R123, R245fa, R290, R600a, and R600, were investigated to determine appropriate working fluid for ORC-VCR system by Bu et al. [15].

They concluded that R600a is the most suitable candidate. A combined ORC with a vehicle air conditioning system using R245fa, R134a, pentane, and cyclopentane as working fluids was studied by Yue et al. [16].

Their results indicated that R134a gives the maximum economic and thermal performance. An ORCVCR system powered by low-grade thermal energy using two different substances for the power and refrigeration cycles was studied by Mole´ s et al. [17].

They concluded that the best candidates for the power and refrigeration cycles are R1336mzz (Z) and R1234ze (E), respectively.From the aforementioned introduction, it is clear that thereis still a need for screening of alternative candidates for ORCVCR system. The present study concentrates on the productionof electricity or cooling

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from low-temperature renewableenergies such as waste heat or geothermal heat having a temperaturearound 100 °C. The potential use of RC318, R236fa, R600a and R245fa as working fluids in the ORC-VCR systemis assessed. The performance of the system is characterized by the COPS and system efficiency.

II. DESCRIPTION OF THE INTEGRATED ORC-VCR SYSTEM

This subsystem consists of a pump, an ORC Evaporator, a Turbine, and condenser (Figure 1). Inthe ORC evaporator, the working fluid is initially heated and then vaporized at ORC evaporationtemperature Teva by means of the heat absorbed from the heat source QORC. Then thesteam generated at high pressure enters the expander, whose enthalpy is converted into power Wt. Then, the fluid enters the condenser, where it condenser at condensation temperature Tcond_ due to the rejection of Qcond to the external medium, which is at temperature To. Next, the working fluid enters the pump, which moves the fluid to the ORC Evaporator to complete the cycle [17].

The net mechanical power provided by the ORC cycle is used to drive the compressor of theVCR cycle. This second subsystem consists of a compressor, a condenser, Expansion valves, and VCRE vaporator (Figure 1).

In the VCR Evaporator, the working fluid absorbs the cooling load Qeva_VCR from the cooling space at the VCR evaporation temperature Tevap_VCR. Then, the working fluid is compressed in the compressor, and in the condenser, the working fluid rejects Qcond at Tcond to the condensing medium which is T0. Finally, it expands in the Expansion valve.

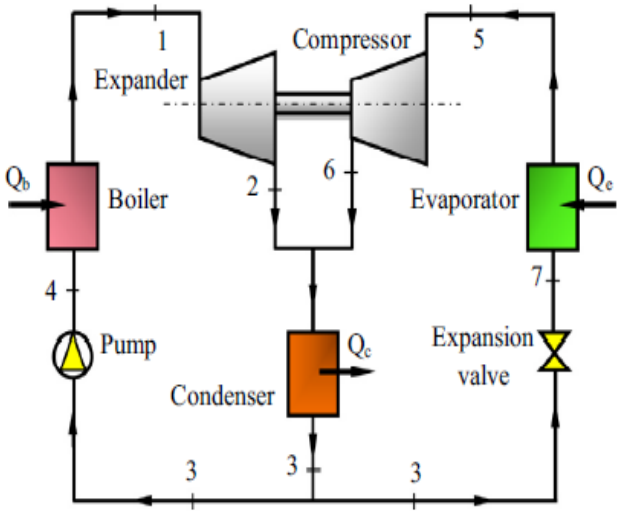

Fig 1. ORC-VCR system schematic diagram.

The selection of working fluid for the ORC-VCR systems is a critical issue, where it plays a key role in the system performance. An appropriate working fluid should achieve both minimal environmental issuesand high system performance. Because of their zero ozone depletion potential (ODP), HFCs and FCs have been considered as working fluids substituting hydrochloro fluoro carbons (HCFCs) and chloro fluoro carbons (CFCs) in VCR cycle, ORC, ejector refrigeration cycle and integrated cycles [2, 22].

Recently, these fluids are regulated due totheir high global warming potential (GWP). Consequently, research isstill ongoing for other fluids, which may have lower environmental issues. Using HCs as alternative working fluids is one possibility. HCs have a very low GWP, environmentally friendly and superior thermo physical properties [23].

The only controversy issue against using HCsis its flamm ability. However, the flamm ability will not constitute the biggest challenge in utilizing HCs with appropriate safety precautions. Also, HFEs have been proposed as alternative working fluids due totheir zero ODP and significantly low GWP.

HFEs have other environmental features such as shorter atmospheric life time (ALT) and lower GWP as compared with HFCs. Also, they are non-flammable and low toxicity [24].

Furthermore, numerous HFOs with low environmental impact are proposed as working fluids [2, 12].

III. MATHEMATICAL MODEL AND COMPUTATIONAL PROCEDURE

The thermodynamic mathematical model for the ORC-VCR system illustrated in Fig. 1 is described as follows:

1. With respect to the ORC:

$$W_{exp}=m_{ORC}(h_1-h_{2a})= m_{ORC}(h_1-h_{2s})\eta_{exp}$$

Where; Wexp is the output power from the expander during process (1-2a) in kW, mORC is the mass flow rate of the working fluid in the ORC in kg/s, h1 is the expander inlet specific enthalpy in kJ/kg, h2a is the expander exit actual specific enthalpy in kJ/kg, h2s is the expander exit isentropic specific enthalpy in kJ/kg, and ηexp is the expander isentropic efficiency.

$$W_{exp}=m_{ORC}(h_{4a}-h_3) = m_{ORC}(h_{4s}-h_3)/\eta_p$$

Where, WP is the inlet power to the pump during process (3-4a) in kW, h4a is the pump exit actual specific enthalpy in kJ/kg, h3 is the pump inlet specific enthalpy in kJ/kg, h4s is the isentropic specific enthalpy at the pump outlet in kJ/kg, and ηP is the pump isentropic efficiency.

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Wnet = Wexp – WP

Where, Wnet is the net output power from the ORC in kW

Qb = mORC (h1 –h4a)

Where, Qb is the heat transfer rate to the working fluid in the boiler during the process (4a-1) in kW, h1 is the boiler outlet specific enthalpy in kJ/kg, and h4a is the boiler inlet actual specific enthalpy in kJ/kg.

ηORC = W_net/Q_b

Where, ηORC is the organic Rankine cycle efficiency.

2. With respect to the VCR cycle:

Qe = mVCR (h5 –h7)

Where, Qe is the rate of heat transfer to the working fluid in the evaporator during process (7-5) in kW, mVCR is the mass flow rate of the working fluid in the VCR in kg/s, h5 is the evaporator outlet specific enthalpy in kJ/kg, and h7 is the evaporator inlet specific enthalpy in kJ/kg.

Wc = mVCR (h5 –h6a) = mVCR (h5 – h6s)/ ηc

Where, Wc is the inlet power to the compressor during process (5-6a) in kW, h5 is the compressor inlet specific enthalpy in kJ/kg, h6a is the compressor outlet actual specific enthalpy in kJ/kg, h6s is the compressor outlet isentropic specific enthalpy in kJ/kg, and ηc is the compressor isentropic efficiency.

Wc = Wnet

The VCR cycle COP is defined as follows:

COPVCR=Qe/Wc

The COPS can be calculated as follows:

COPs = ηORC COPVCR

The compressor compression ratio (CMR) during the process (5-6a) and the expander expansion ratio (EPR) during the process (1-2a) are measures for the required compressor and expander sizes, respectively, and described as follows:

CMR= P6a/P5

EPR = v2a/v1

The basic values of the ORC-VCR system operating parameters and their ranges are presented in Table 1. EES code was established to assess the ORC-VCR system performance as well as the CMR and EPR with various candidates under different working conditions.

Table 1. The basic values of the parameters utilized in the ORC-VCR system and their ranges.

Parameter	Touaibi et. al. (2018)	Present
Mass flow rate of the working fluid in ORC	1 Kg/s	-
Isentropic efficiency of the feed pump	85%	-
Boiler temperature	80°C	60-105 °C
Isentropic efficiency of the expander	80%	-
Condenser temperature	40°C	30-55 °C
Evaporator temperature	80°C	-15 to 15 °C
Isentropic efficiency of the compressor	85%	-

IV. RESULTS AND DISCUSSION

In this work, the performance of ORC-VCR system using four refrigerants, i.e. RC318, R236fa, R600a and R245fa as working fluids was calculated and analysed.

1. EES Code Validation:

To validate the present model, the simulation results have been compared with the available numerical data in the literature using the R600a as working fluid. The results of this study were compared with the simulation data published by Touaibi (2018).

Table 4.1 presents the combined system performances for the same operating conditions used by Touaibi 2018). According to comparison, the agreement between the two simulation results is good.

Table 2. Validation of the model with the results of the Touaibi (2018).

Parameter	Touaibi (2018)	Present
η_{ORC}	0.0789	0.0971
COP_{VCR}	5.12	7.518
η_s	0.49	0.725
COPs	0.40	0.73

Table 3. Performances of the combined system ORC-VCR according to the studied working fluids.

Parameter	R600a	RC318	R245fa	R236fa
η_s	0.6654	0.5445	0.6798	0.6464
COP_s	0.73	0.6144	0.7458	0.7107
CMR	2.192	1.522	2.88	2.403
EPR	3.538	6.859	4.299	4.459

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The results in Table 3 shows that among all candidates, R600 and R245fa with the highest critical temperatures have the maximum and the same COPS values, whereas RC318, R1234yf, and R1270 with the lowest critical temperatures have the minimum COPS values.

2. Influence of Boiler Temperature on the System Performance:

The effect of boiler temperature on the ORC-VCR system performance with different candidates, are presented in below figures.

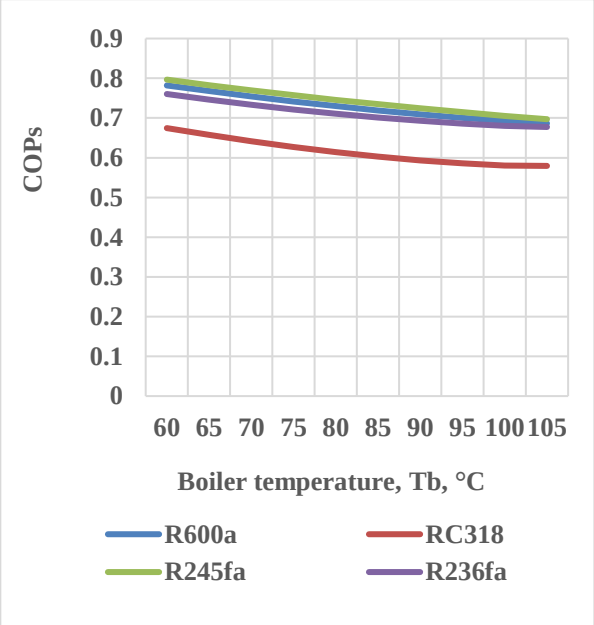

Fig 2. The effect of boiler temperature on the COPS for various candidates in the basic ORC-VCR system.

Fig 2. displays the alteration in COPS as a function of the boiler temperature for different candidates in the basic ORC-VCR system. This figure shows that the COPS of the system decreases as the boiler temperature increases for all candidates. Among the proposed working fluids, R245fa achieve the highest COPS for all boiler temperatures, while RC318, R600a, and R236fa attain the lowest COPS.

The variation of ηsys as a function of Tb for all candidates in the typical system is displayed in Fig. 3. As can be observed from the figure, the increase of Tb leads to a decrease in system efficiency, ηsys. Among the proposed working fluids, R245fa achieve the highest system efficiency for all boiler temperatures, while RC318 attain the lowest system efficiency.

Fig. 4 exhibits the change in CMR values as a function of the boiler temperature for different candidates in the basic ORC-VCR system. This figure shows that the CMR decreases as the boiler temperature increases for all candidates. This is due to the rise of saturation pressure with the temperature.

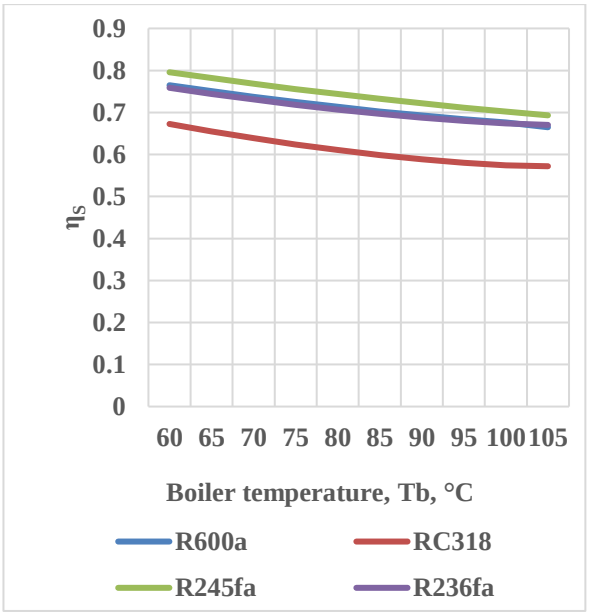

Fig 3. The effect of boiler temperature on the system efficiency for various candidates in the basic ORC-VCR system.

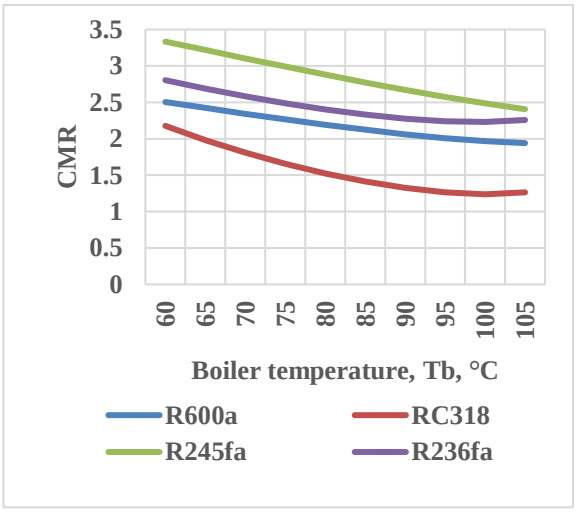

Fig 4. The effect of boiler temperature on the CMR for various candidates in the basic ORC-VCR system.

The CMR values at a boiler temperature of 90°C are nearly twice those at 60 °C for all candidates. The maximum CMR is achieved by R245fa. The minimum CMR is attained by RC318, R600a and R236fa.Fig. 5 exhibits the change in EPR values as a function of the boiler temperature for different candidates in the basic ORC-VCR system.

This figure shows that the EPR increases as the boiler temperature increases for all candidates. This is due to the rise of saturation pressure with the temperature. The EPR values at a boiler temperature of 90°C are nearly twice those at 60 °C for all candidates. The maximum EPR is achieved by RC318fa. The minimum EPR is attained by R245fa, R600a and R236fa.

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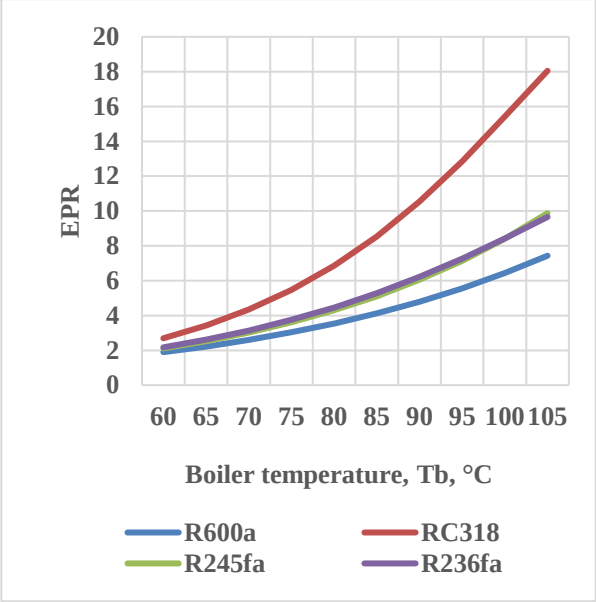

Fig 5. The effect of boiler temperature on the EPR for various candidates in the basic ORC-VCR system.

3. Influence of Condenser Temperature on the System Performance:

The variation of COPS with the condenser temperature for all candidates in the basic ORC-VCR system is illustrated in Fig. 6-9.

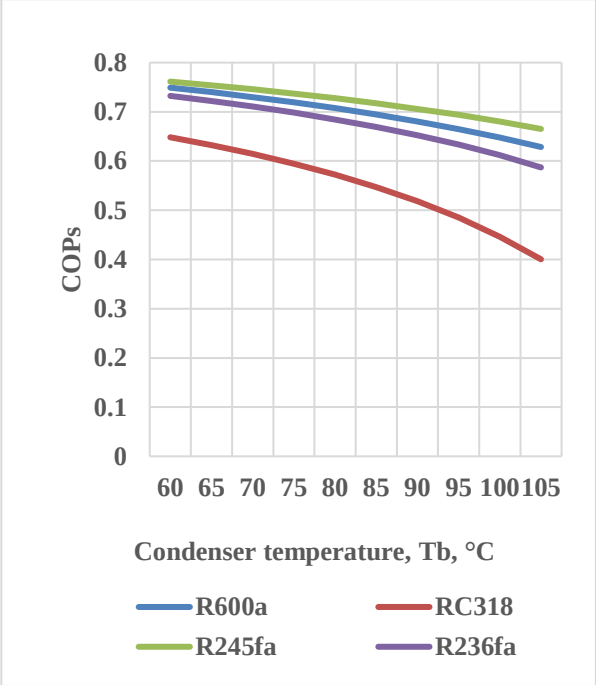

Fig 6. The effect of condenser temperature on the COPS for various candidates in the basic ORC-VCR system.

It is observed from the figure that, the condenser temperature has a large effect on the COPS. This is because the condenser temperature has an effect on both VCR cycle and ORC individually. The rejected heat is governed by condenser temperature, which is an additional parameter to boost the cycle efficiency in addition to the boiler temperature.

Small values of rejected heat are preferable to achieve high efficiencies in both cycles. It can be noticed from Fig. 7 that the COPS reduces with the increase in condenser temperature for all candidates. This is justified by the truth that as the temperature and pressure kept constant at the inlet of the compressor, the increase in condenser temperature causes the rise of pressure and enthalpy at the compressor exit.

Among the proposed working fluids, R245fa achieve the highest COPs values for all condenser temperatures, while RC318 attains the lowest COPS.

The variation of system efficiency with the condenser temperature for various candidates in the basic ORC-VCR system is displayed in Fig. 8. Generally, the increase in condenser temperature leads to decrease of system efficiency for all candidates. RC318 attained the lowest system efficiency, while the highest was achieved by R245fa for all condenser temperatures.

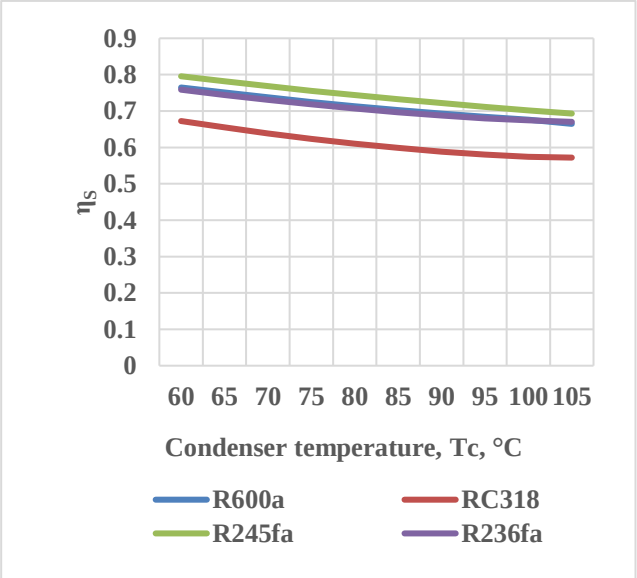

Fig 7. The effect of condenser temperature on the system efficiency for various candidates in the basic ORC-VCR system.

The influences of condenser temperature on the CMR for different working fluids in ORC-VCR system are illustrated in Fig. 9, respectively. It is detected from these figures that with the increase in condenser temperature, the CMR increases. This is logically when taking into account the thermos-physical properties effect of these candidates.

The variations between the CMR values for the proposed working fluids are smaller at low than that at high condenser temperatures.

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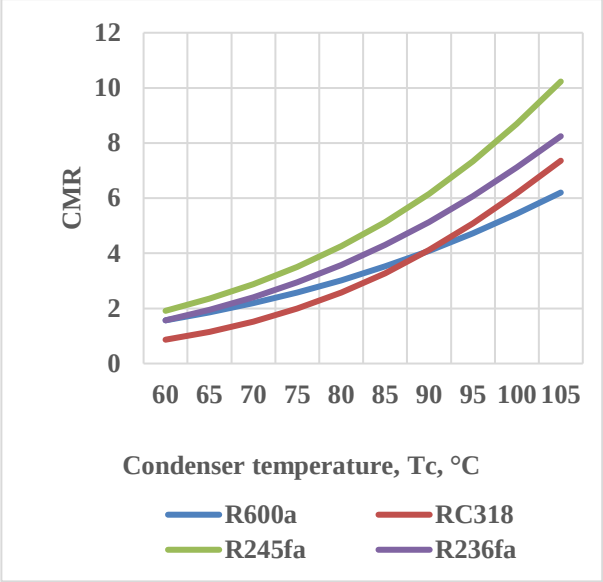

Fig 8. The effect of condenser temperature on the CMR for various candidates in the basic ORC-VCR system.

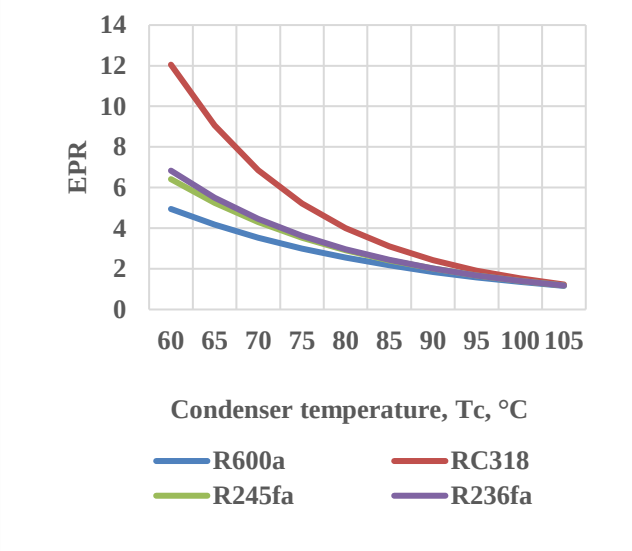

Fig 9. The effect of condenser temperature on the EPR for various candidates in the basic ORC-VCR system.

The influences of condenser temperature on the EPR for different working fluids in ORC-VCR system are illustrated in Fig. 10, respectively. It is detected from these figures that with the increase in condenser temperature, the EPR decreases. This is logically when taking into account the thermos-physical properties effect of these candidates. The variations between the EPR values for the proposed working fluids are smaller at high than that at low condenser temperatures.

4. Influence of Evaporator Temperature on the System Performance:

The variation of COPS with the condenser temperature for all candidates in the basic ORC-VCR system is illustrated in below Figures.

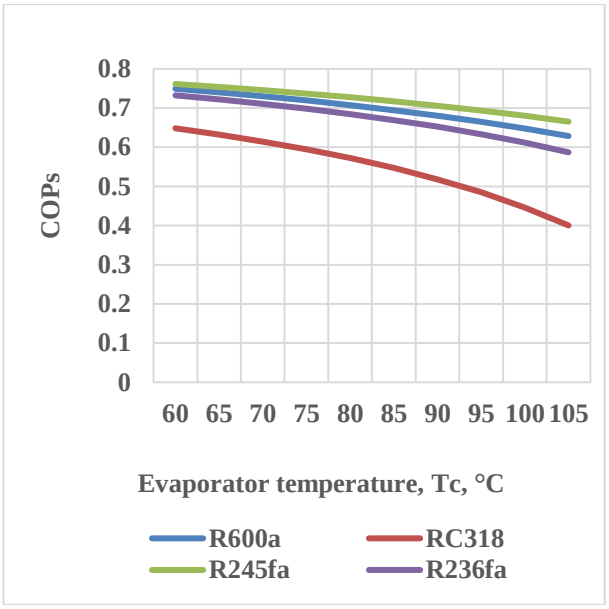

Fig 10. The effect of evaporator temperature on the COPS for various candidates in the basic ORC-VCR system

It can be noticed from Fig. 11 that, the increment in evaporator temperature leads to decrement of the COPS. This can be interpreted by the truth that with the increase in evaporator temperature its saturation pressure decreases. Among the proposed candidates, R245fa attain the highest COPs values, while R600, RC318 and R236fa has the lowest COPs values for all evaporator temperatures.

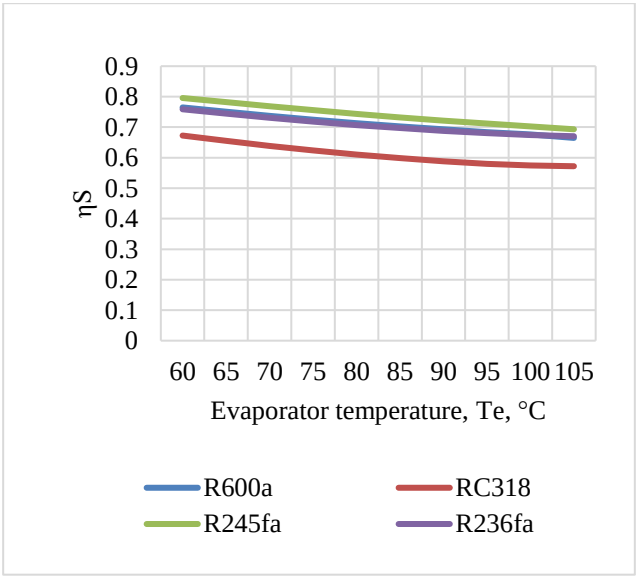

Fig 11. The effect of evaporator temperature on the system efficiency for various candidates in the basic ORC-VCR system.

It can be noticed from Fig. 12 that, the increment in evaporator temperature leads to decrement of the system efficiency. This can be interpreted by the truth that with the increase in evaporator temperature its saturation pressure decreases. Among the proposed candidates,

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R245fa attain the highest system efficiency values, while R600, RC318 and R236fa has the lowest system efficiency values for all evaporator temperatures.The variation of CPR as a function of Teva for all candidates in the typical system is presented in Fig. 13.

The general trend in the figure is an increase of CMR with the increase of Teva. This is because of the evaporator pressure decreases as Teva rises, which leads to an increase in CMR at constant Tc. The increase in CMR leads to a decline in the required Ẇcomp which results in a decrease in CPOs.

Accordingly, form the energetic viewpoint, to get maximum COPs the CMR should be minimum. Among all candidates, R245fa attains the maximum CMR values while RC318 achieves the minimum values for all studied Teva.

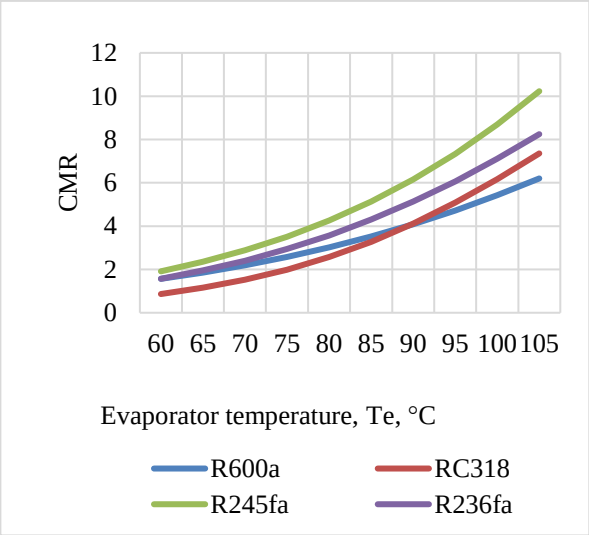


Fig 12. The effect of evaporator temperature on the CMR for various candidates in the basic ORC-VCR system.

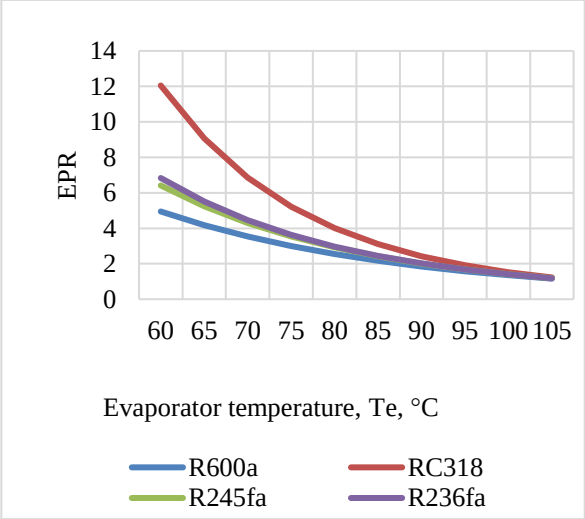


Fig 13. The effect of evaporator temperature on the EPR for various candidates in the basic ORC-VCR system.

The variation of EPR as a function of Teva for all candidates in the typical system is presented in Fig. 14. The general trend in the figure is a decline of EPR with the increase of Teva. This is because of the evaporator pressure increases as Teva rises, which leads to a decrease in EPR at constant Tc.

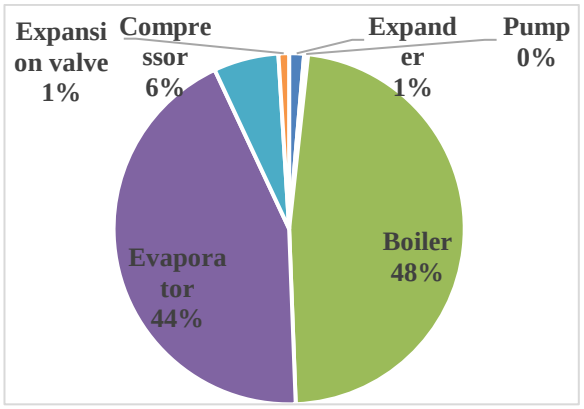
The decrease in EPR leads to a decline in the required Ẇcomp which results in an increase in CPOs. Among all candidates, RC318 attains the maximum EPR values while R600a achieves the minimum values for all studied Teva.

5. Exergy Destruction Distribution in the Combined System ORC-VCR:

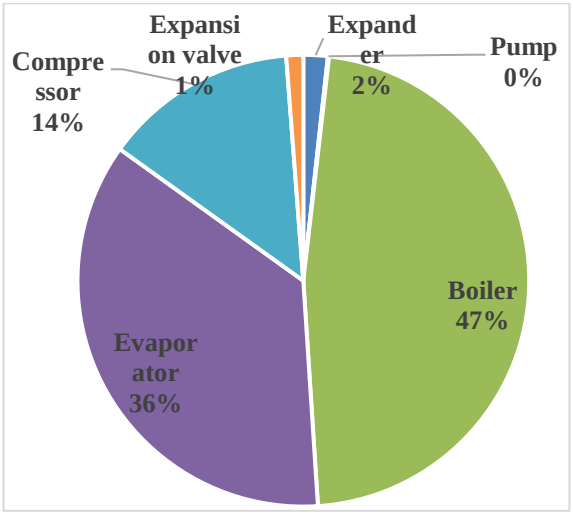
The exergy destruction ratio is a beneficial parameter for comparison of exergy destruction among different system components and to determine the weak points of a system.

The total destroyed exergy rate is 578.3 kW (R600a), 201.5 kW (RC318), 340.3 (R245fa) and 261.8 (R236fa).

By comparing the exergy destruction proportion for each component of the system, it is clear that the largest amount of destroyed exergy occurs in the boiler.



(a) R600a



(b) RC318

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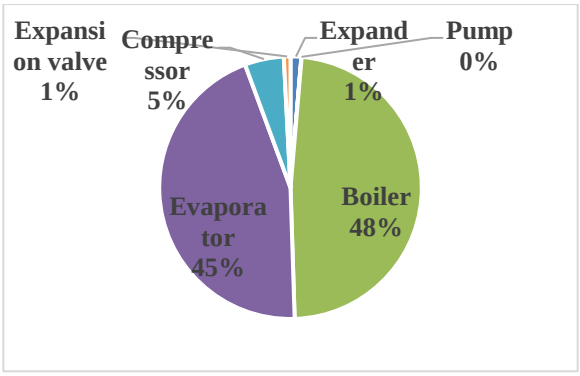
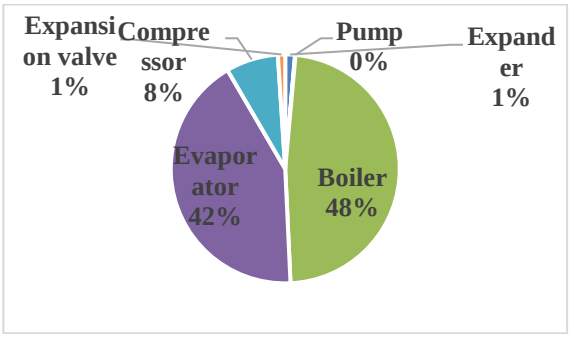


(c) R245fa



(d) R236fa

Fig 14. Exergy destruction distribution in the system according to the studied working fluids.

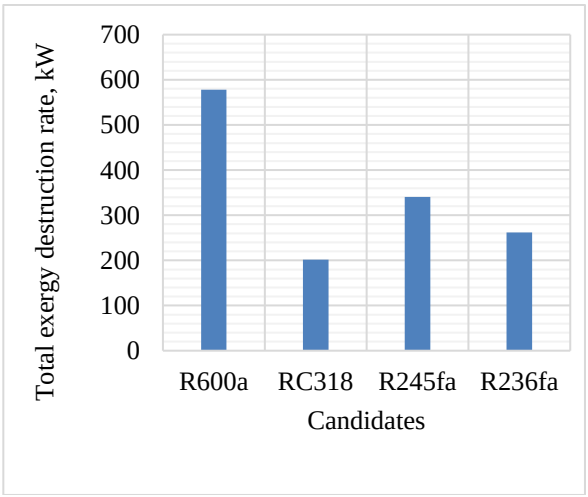


Fig 15. Total exergy destruction rate in the system according to the studied working fluids.

It is cleared the maximum total exergy destruction rate is found in R600a and minimum is in RC318.

V. CONCLUSION

In the present research, the performance of ORC-VCR system activated by low-grade thermal energy is investigated. Some common refrigerants such as RC318, R236fa, R600a and R245fa are proposed as working fluids. The effects of evaporator, condenser, and boiler temperatures on the ORC-VCR system performance are also examined and discussed.

The results indicate that all studied parameters have comparable influences on the ORC-VCR system performance for all candidates. In detail, as the evaporator, condenser and boiler temperatures increase, the COPs decreases for all candidates. Also, as the evaporator, condenser and boiler temperatures increase, the system efficiency decreases for all candidates.

Also, as the evaporator and boiler temperatures increase, the compression ratio increases and the expansion ratio increases, respectively, while the reverse occurs with the condenser temperature. From the acquired results it can be concluded that, among all candidates, R600a achieve the highest COPs values. The distribution of exergy destruction shows that for the four studied fluids, most of the exergy is destroyed at the boiler followed by at the ORC evaporator and condenser.

The exergy destruction ratio is a beneficial parameter for comparison of exergy destruction among different system components and to determine the weak points of a system. The total destroyed exergy rate is 578.3 kW (R600a), 201.5 kW (RC318), 340.3 (R245fa) and 261.8 (R236fa).

Due to environmental issues of R600a is recommended as a superior candidate for the ORC-VCR system for retrieving low-grade thermal energy.

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